



UTM
UNIVERSITI TEKNOLOGI MALAYSIA

OPENCOURSEWARE

Thermodynamics II

Chapter 3

Compressors

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Coverage

- Introduction
- Indicated Work, Mechanical Efficiency
- Condition for Minimum Work
- Isothermal Efficiency
- Compressors with Clearance
- Volumetric Efficiency, Free Air Delivery
- Multistage Compression
- Ideal Intermediate Pressure

Introduction

- Compressed air is air kept under a pressure that is greater than atmospheric pressure.



- In industry, compressed air is so widely used that it is often regarded as the fourth utility, after electricity, natural gas and water.

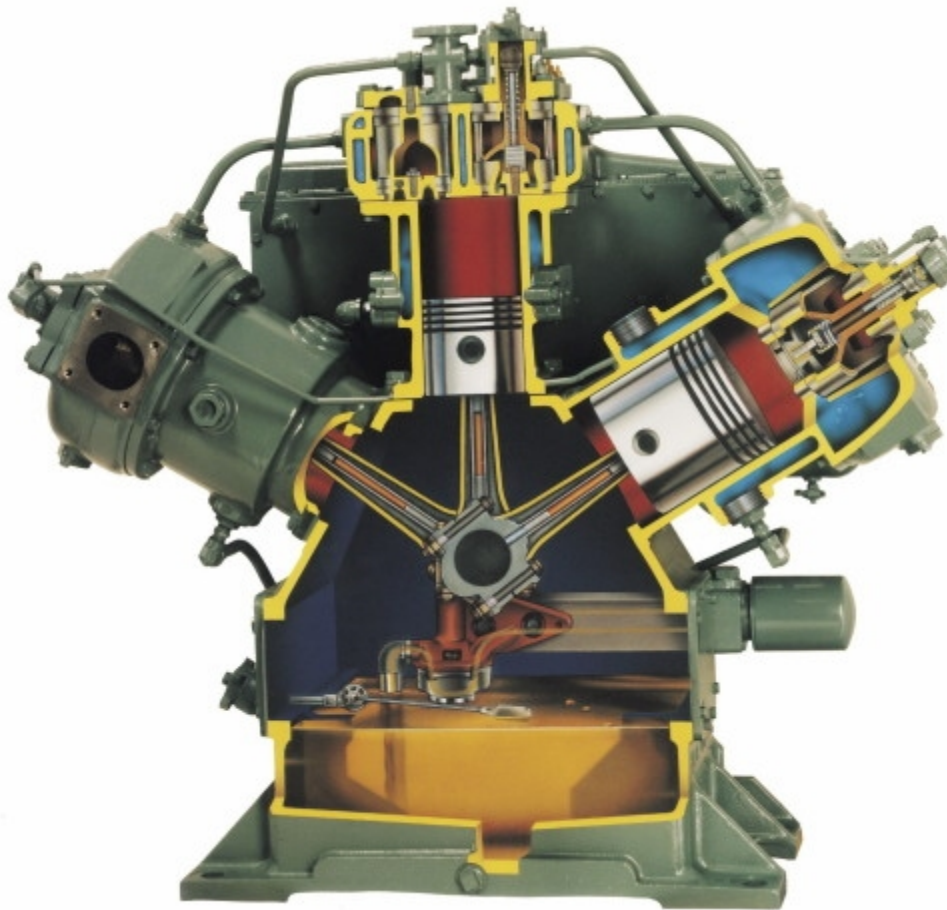
Usages

Compressed air is used for many purposes, including:

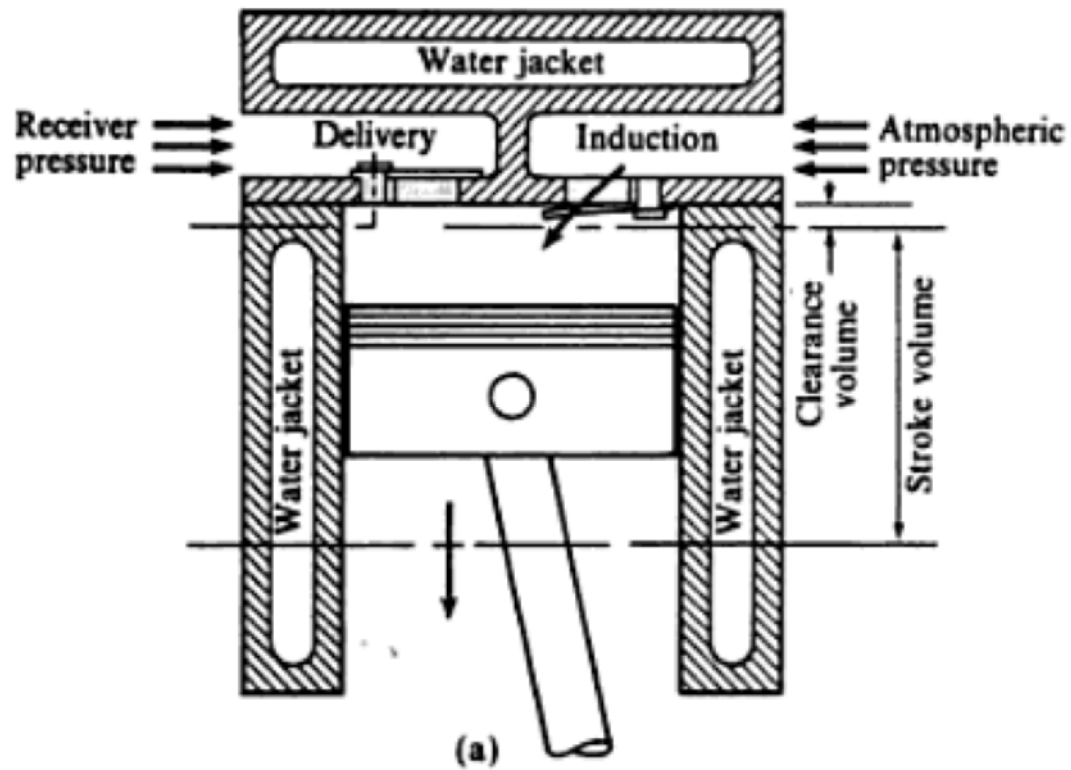
- Pneumatics, the use of pressurized gases to do work
 - Pneumatic post, using capsules to move paper and small goods through tubes.
 - Air tools
 - HVAC control systems
- Vehicle propulsion (compressed air vehicle)
- Energy storage (compressed air energy storage)
- Air brakes, including:
 - railway braking systems
 - road vehicle braking systems
- Scuba diving, for breathing and to inflate buoyancy devices
- Refrigeration using a vortex tube
- Gas dusters for cleaning electronic components that cannot be cleaned with water
- Air-start systems in engines
- Ammunition propulsion in:
 - Air guns, Airsoft equipment, Paintball equipment

Compressor types

- **Positive Displacement Machines**
(high pressure ratio, low mass flow rates)
 - Rotating
 - Screw compressors (Lysholm)
 - Scroll compressor
 - Roots blowers
 - Alternating (Reciprocating Compressor)
- **Turbocompressors**
(low pressure ratio, high mass flow rates)
 - Centrifugal compressor
 - Axial compressor
 - Mixed-flow compressor

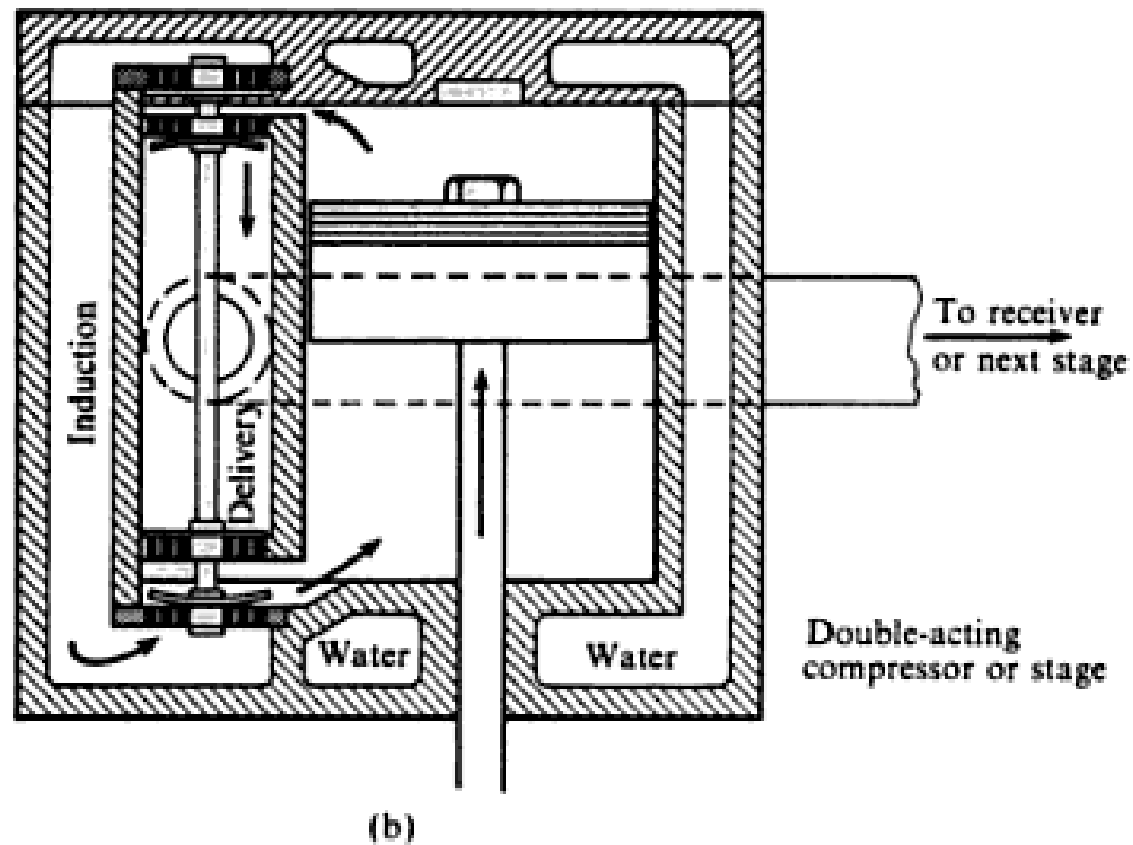


Reciprocating Compressor



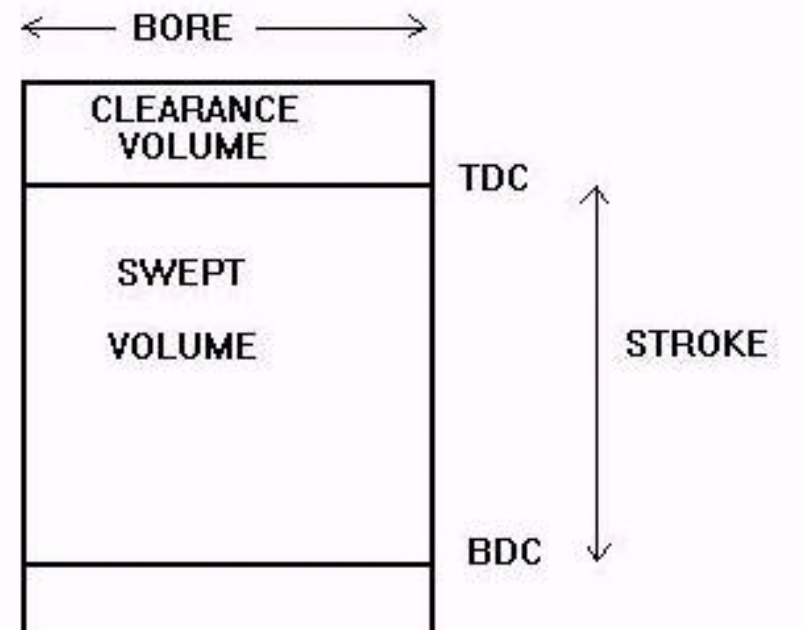
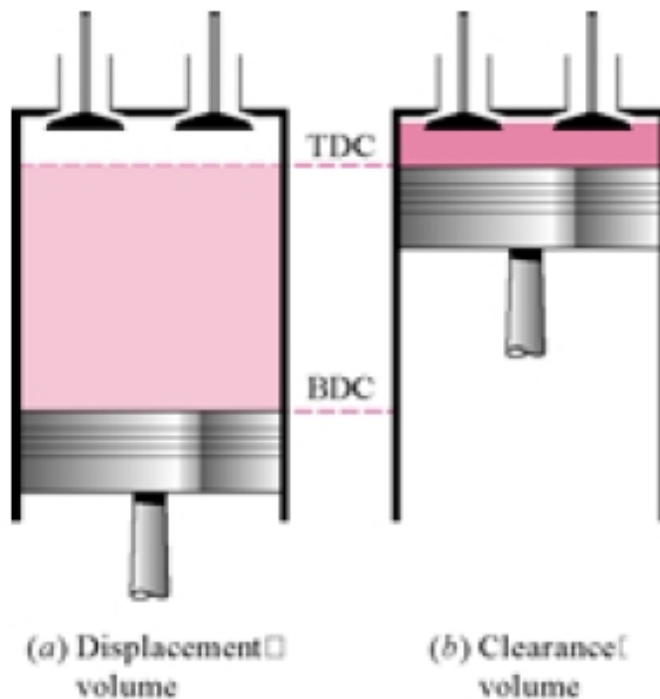
Single Acting

Reciprocating Compressor



Double Acting

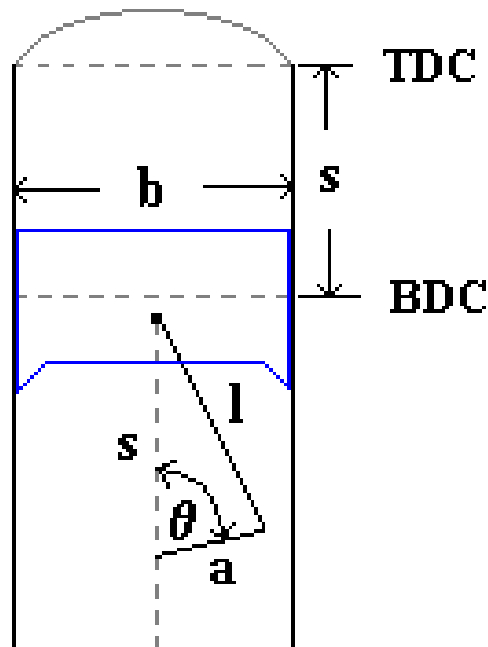
Piston-cylinder terminologies



TDC – Top Dead Center

BDC – Bottom Dead Center

Piston-cylinder terminologies



b – Bore, Diameter

s – Stroke

l – Connecting Rod Length

a – Crank Throw = $\frac{1}{2}$ stroke

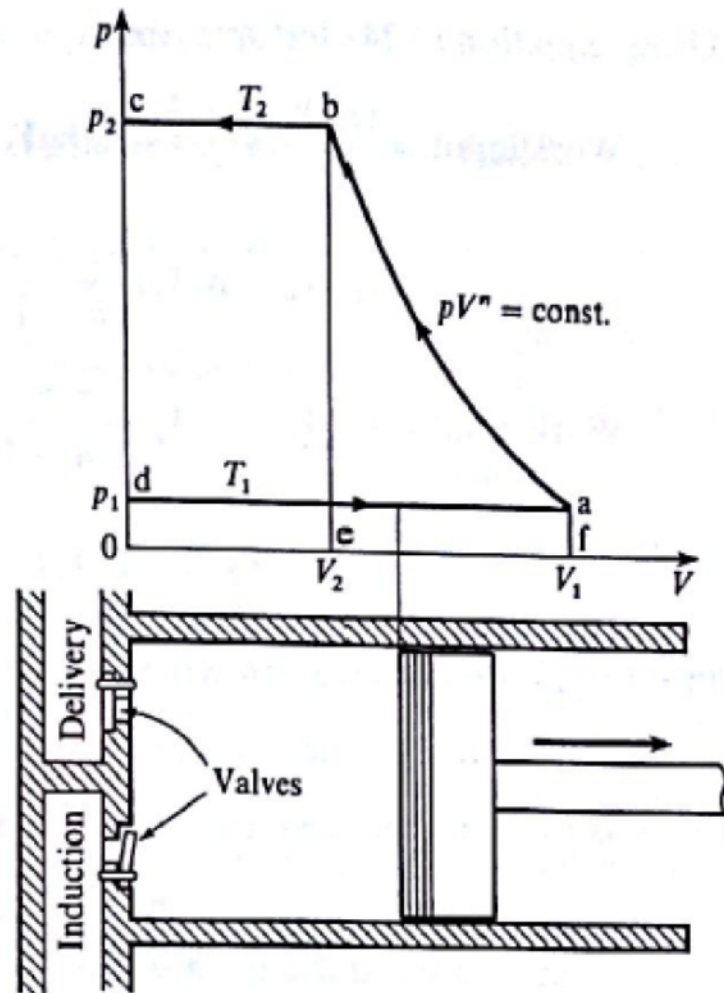


Fig. 12.2 Pressure–volume diagram for a reciprocating compressor with clearance neglected

$$\frac{P_2}{P_1} = \text{Pressure Ratio} = r_p$$

Compressor Operation

- Process d – a : Intake or Induction
 - Piston moves from TDC to BDC
 - Intake valve opens and air induced into cylinder
 - Pressure P_1 and temperature T_1 remain constant.
- Process a – b : Compression
 - Intake valve closes and piston moves towards TDC
 - Compression follows the polytropic process $Pv^n=c$ until P_2 is reached.

Compressor Operation

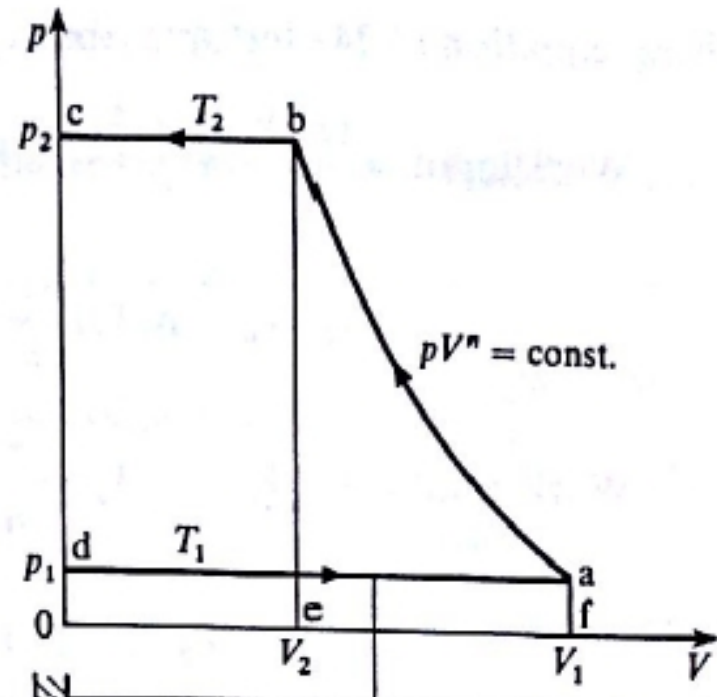
- Process b – c : Delivery
 - Delivery valve opens
 - Compressed air exits and delivered.
 - Pressure P_2 and temperature T_2 remain constant.
- Process c – d : Expansion
 - Both valves remain closed as the cycle returns to the initial state
 - Constant volume if without clearance
 - Polytropic expansion if with clearance

Indicated Work

- Indicated by P-v diagram, (P-v diagram = Indicator diagram)

For a cycle

$$\begin{aligned}
 W_{ind} &= \int_1^2 P dV \\
 &= \text{area of abcd} \\
 &= \text{abef} + \text{bcoe} - \text{adof} \\
 &= \frac{P_2 V_b - P_1 V_a}{n-1} + P_2 V_b - P_1 V_a \\
 &= \frac{n}{n-1} (P_2 V_b - P_1 V_a)
 \end{aligned}$$



Recall polytropic relationship between two states

$$\frac{T_2}{T_1} = \left(\frac{P_2}{P_1} \right)^{\frac{(n-1)}{n}} = \left(\frac{v_1}{v_2} \right)^{(n-1)}$$

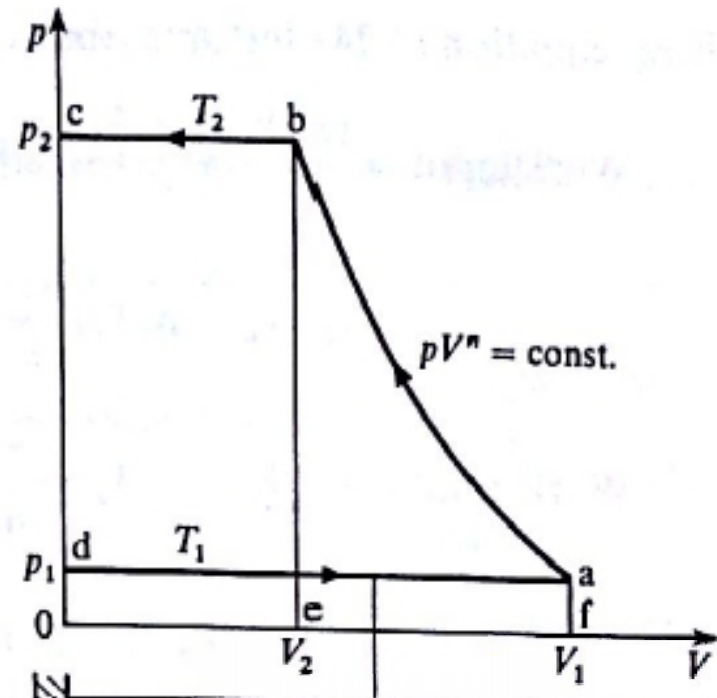
Indicated Work

Can also be considered as open system

$$\begin{aligned}
 W_{ind} &= \int_{P_1}^{P_2} V dP \\
 &= \text{area of abcd} \\
 &= \frac{n}{n-1} (P_2 V_b - P_1 V_a)
 \end{aligned}$$

And since $PV = mRT$

$$\begin{aligned}
 W_{ind} &= \frac{n}{n-1} (mRT_2 - mRT_1) \\
 &= \frac{n}{n-1} mR(T_2 - T_1) \\
 &= \frac{n}{n-1} mRT_1 \left(\frac{T_2}{T_1} - 1 \right)
 \end{aligned}$$



$$\begin{aligned}
 &= \frac{n}{n-1} mRT_1 \left(\left(\frac{P_2}{P_1} \right)^{\frac{n-1}{n}} - 1 \right) \\
 &= \frac{n}{n-1} P_1 V_a \left(\left(\frac{P_2}{P_1} \right)^{\frac{n-1}{n}} - 1 \right)
 \end{aligned}$$

Power (and Rates)

- Has to take into account single or double acting
- W_{ind} is work per cycle of P-v diagram.
- If single acting, one cycle per crank revolution
- If double acting, two cycles per crank revolution (one cycle each for both sides of piston face).
 - Mass flow rate is doubled accordingly.

$$\begin{aligned}\dot{W} &= \frac{n}{n-1} \dot{m} R T_1 \left(\left(\frac{P_2}{P_1} \right)^{\frac{n-1}{n}} - 1 \right) \\ &= \frac{n}{n-1} P_1 \dot{V} \left(\left(\frac{P_2}{P_1} \right)^{\frac{n-1}{n}} - 1 \right)\end{aligned}\quad \dot{m} = m \times N \times \text{action}$$

Mechanical Efficiency

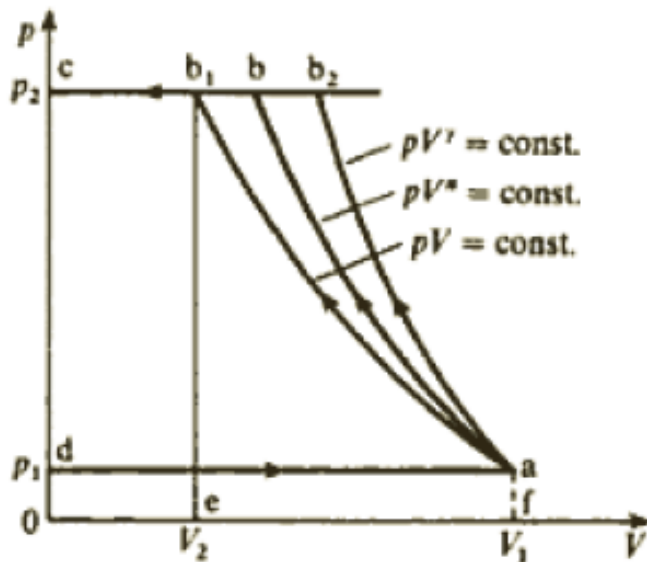
- The actual power input into the compressor is larger than the indicated power, to overcome friction and other losses.

Shaft power = Indicated power + Friction power loss

$$\text{Mechanical Efficiency} = \frac{\text{Indicated power}}{\text{shaft power}}$$

Other losses can also be taken into account accordingly

Condition for Minimum Work



- We aim to reduce the input work
- d-a is the stroke, determined by cylinder design and measurement
- P_2 is desired delivery pressure. As long as P_2 is reached, the compressor has done its job.

- Only the compression process can be adjusted by varying n , the polytropic index.
- Isothermal process ($n=1$) results in minimum work (smallest area).
- Compressors are cooled by water jackets or cooling fins

Isothermal Work, Isothermal Efficiency

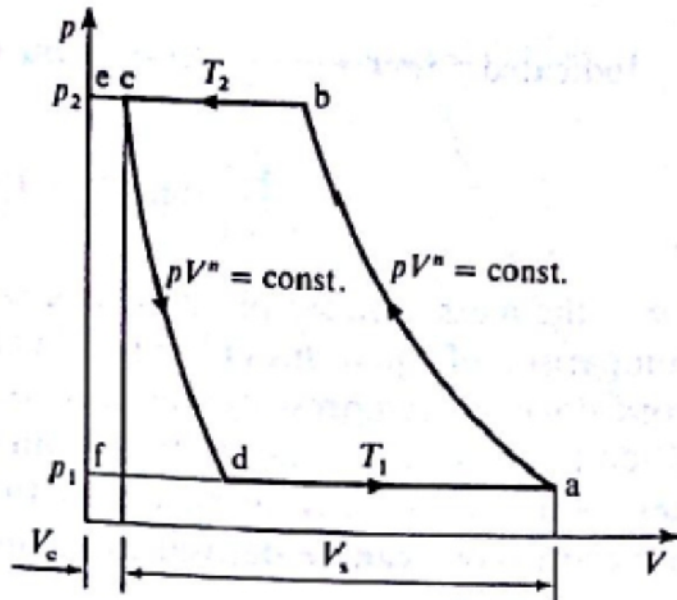
- Integrating by isothermal process, $Pv=c$

$$\begin{aligned} W_{\text{isothermal}} &= P_1 V_a \ln \left(\frac{P_2}{P_1} \right) \\ &= mRT \ln \left(\frac{P_2}{P_1} \right) \end{aligned}$$

- Isothermal efficiency

$$\eta_{\text{isothermal}} = \frac{\text{Isothermal Work}}{\text{Indicated Work}}$$

Compressors with Clearance



- Clearance is needed for free movements of piston and valves
- Clearance volume is V_c .
- When delivery is completed (b-c), there is still compressed air at P_2 and T_2 in the clearance volume.

- When intake stroke begins at V_c , no outside air can enter yet until the residual compressed air has expanded down to P_1 and T_1 .
- Thus, *having clearance reduces the volume of inducted air from $(V_a - V_c)$ originally to only $(V_a - V_d)$*

Compressors with Clearance

- Mass of air, $m_a = m_b$, and $m_d = m_c$
- The amount of air handled, $m = m_a - m_d = m_b - m_c$
- $W_{ind} = \text{area abcd}$
 $= \text{area abef} - \text{area cefd}$

$$\begin{aligned}W_{ind} &= \frac{n}{n-1} m_a R (T_2 - T_1) - \frac{n}{n-1} m_d R (T_2 - T_1) \\&= \frac{n}{n-1} (m_a - m_d) R (T_2 - T_1) \\&= \frac{n}{n-1} m R (T_2 - T_1)\end{aligned}$$

Even though Work depends on clearance, but *work per unit mass* does not depend on it.

Free Air Delivery, FAD

- FAD is the amount of air handled (delivered) by the compressor.
- FAD is given as the volumetric flow rate of air (measured at free air conditions P_o and T_o)

$$\text{FAD} = \dot{V}_u = \frac{\dot{m}RT_o}{P_o}$$

Actually, this is easier given by the mass flow rate since it does not depend on P and T

Volumetric Efficiency

$$\eta_v = \frac{m_u}{m_s}$$

The mass of gas entering

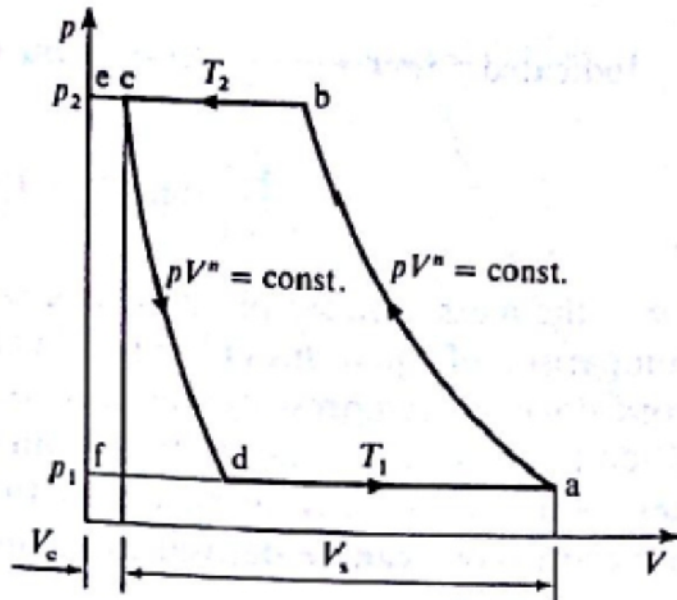
The mass of gas that should fill the swept volume at the same reference condition (free air condition)

$$\eta_v = \frac{V_u}{V_s}$$

The volume of gas entering measured at free air condition

The swept volume of cylinder

Volumetric Efficiency



$$\eta_v = \frac{V_u}{V_s} = \frac{(V_a - V_d)}{(V_a - V_c)}$$

$$\eta_v = 1 - \frac{V_c}{V_s} \left[\left(\frac{P_2}{P_1} \right)^{1/n} - 1 \right]$$

- The result above is assuming that the in-cylinder condition (T_1, P_1) is the same as free air condition (T_o, P_o)

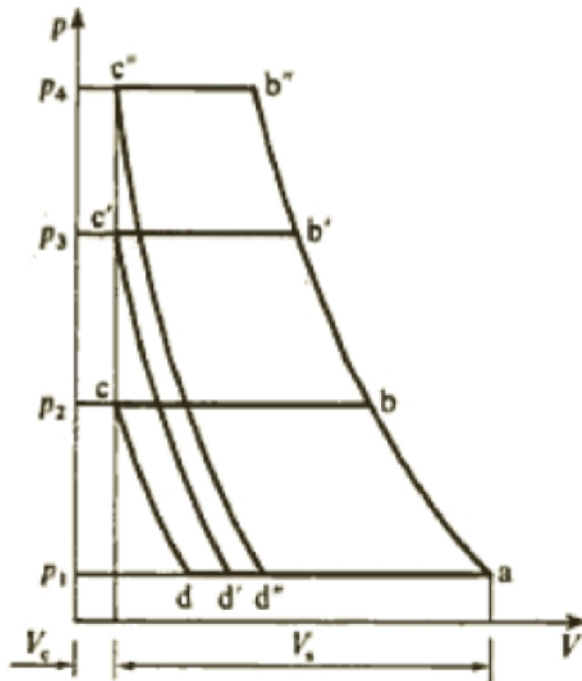
Volumetric Efficiency

- The entering air is actually being heated by the hot cylinder walls and there has to be a pressure difference ($P_o - P_1$) so that air can flow into the cylinder.
- We can use the unchanging mass to get the correction factor to account for these differences

$$V_u = (V_a - V_d) \frac{T_o}{T_1} \frac{P_1}{P_o}$$

$$\eta_v = \left\{ 1 - \frac{V_c}{V_s} \left[\left(\frac{P_2}{P_1} \right)^{1/n} - 1 \right] \right\} \frac{T_o}{T_1} \frac{P_1}{P_o}$$

Multistage Compression



- For a given V_s , increasing r_p will
 - decrease η_v .
 - Increase delivery temperature
 - To achieve high pressures while avoiding those problems
 - Do Multistage Compression
-
- At some intermediate pressure P_i , the gas is sent to a smaller cylinder to be compressed further.
 - This also allows us to cool the gas (intercooling) to reduce compression work.

Multistage Compression

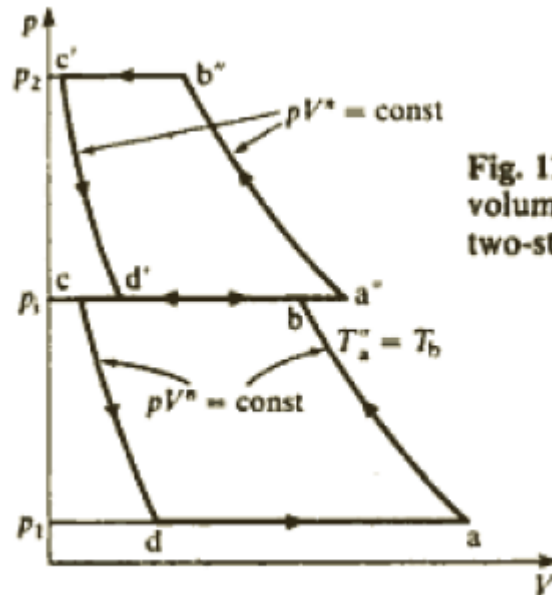


Fig. 12.13 Pressure-volume diagram for two-stage compression

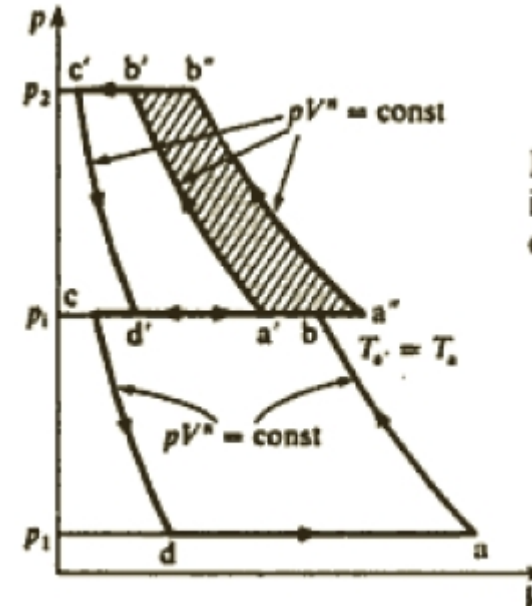
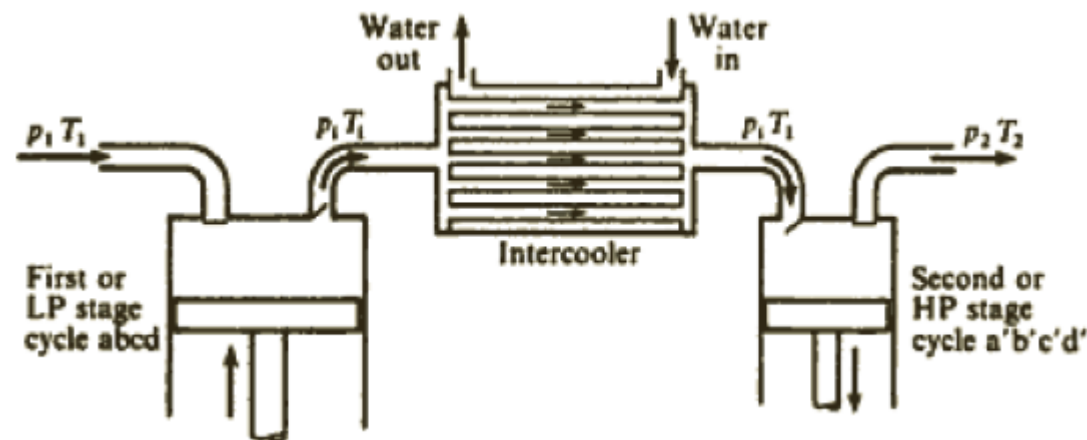


Fig. 12.14 Effect of intercooling on the compression work



Multistage Compression

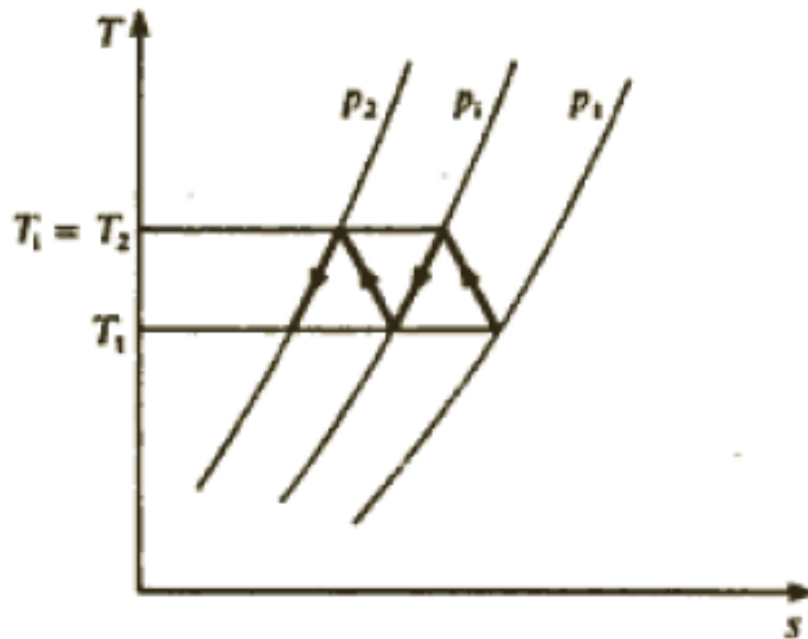


Fig. 12.16 $T-s$ diagram showing intercooling and aftercooling

- Complete Intercooling if
 - Intermediate temperature T_i is cooled back to the same temperature as T_1 .

Optimum Intermediate Pressure

- The chosen P_i affects the amount of compression work that has to be supplied.
- An optimum P_i will give us the minimum compressor work.
- Let's assume complete intercooling.

$$W_{\text{total}} = W_{\text{Low Stage}} + W_{\text{High Stage}}$$

$$W_{\text{Total}} = \frac{n}{n-1} mRT_1 \left(\left(\frac{P_i}{P_1} \right)^{\frac{n-1}{n}} - 1 \right) + \frac{n}{n-1} mRT_i \left(\left(\frac{P_2}{P_i} \right)^{\frac{n-1}{n}} - 1 \right)$$

Since $T_i = T_1$,

$$W_{\text{Total}} = \frac{n}{n-1} mRT_1 \left(\left(\frac{P_i}{P_1} \right)^{\frac{n-1}{n}} + \left(\frac{P_2}{P_i} \right)^{\frac{n-1}{n}} - 2 \right)$$

Optimum Intermediate Pressure

- For a fixed P_1 , T_1 and P_2 , we can find the optimum P_i that gives us minimum W_{total} by

$$\frac{dW_{\text{Total}}}{dP_i} = 0$$

$$\frac{dW_{\text{Total}}}{dP_i} = \frac{d}{dP_i} \left(\frac{n}{n-1} mRT_1 \left(\left(\frac{P_i}{P_1} \right)^{\frac{n-1}{n}} + \left(\frac{P_2}{P_i} \right)^{\frac{n-1}{n}} - 2 \right) \right) = 0$$

$$= \frac{d}{dP_i} \left(\left(\frac{P_i}{P_1} \right)^{\frac{n-1}{n}} + \left(\frac{P_2}{P_i} \right)^{\frac{n-1}{n}} - 2 \right) = 0$$

$$P_i^2 = P_2 P_1$$

$$P_{i-\text{optimum}} = \sqrt[2]{P_2 P_1}$$

$$\frac{P_i}{P_1} = \frac{P_2}{P_i} = r_{p-\text{optimum}} = \left(\frac{P_2}{P_1} \right)^{\frac{1}{2}}$$

Optimum Intermediate Pressure

- So, for minimum compressor work
 - Complete intercooling
 - Same pressure ratio for all stages
- This can be generalized to more than two stages

$$W_{Total} = \frac{n}{n-1} mRT_1 \left(\left(\frac{P_i}{P_1} \right)^{\frac{n-1}{n}} - 1 \right) + \frac{n}{n-1} mRT_i \left(\left(\frac{P_2}{P_i} \right)^{\frac{n-1}{n}} - 1 \right)$$

$$W_{Total} = \frac{2n}{n-1} mRT_1 \left(\left(\frac{P_i}{P_1} \right)^{\frac{n-1}{n}} - 1 \right)$$

$$W_{Total} = \frac{2n}{n-1} mRT_1 \left(\left(\frac{P_2}{P_1} \right)^{\frac{n-1}{2n}} - 1 \right)$$

Optimum Intermediate Pressure

- This can be generalized to more than two stages (z = number of stages, P_1 = intake pressure, P_2 = final pressure)
 - For minimum compressor work
 - Complete intercooling
 - Same pressure ratio for all stages
- $$r_{p-optimum} = \left(\frac{P_2}{P_1} \right)^{\frac{1}{z}}$$

$$W_{Total} = \frac{zn}{n-1} mRT_1 \left(\left(\frac{P_2}{P_1} \right)^{\frac{n-1}{zn}} - 1 \right)$$